AMENDMENTS TO THE SPECIFICATION

Please amend the Specification by inserting on page 1, after the title

--CROSS REFERENCE TO RELATED APPLICATIONS

This application is a Continuation of U.S. Patent Application Serial No. 10/270,212 filed October 11, 2002 which is a Continuation of U.S. Patent Application Serial No. 09/884,261, filed June 19, 2001, now Patent No. US 6,548,611 B2 which is a Continuation of Application Serial No. 08/925,827, filed on September 5, 1997, now abandoned, which is a Continuation of Application Serial No. 08/730,766, filed on October 16, 1996, now Patent No. 5,665,800, which is a Continuation of Application Serial No. 08/606,633, filed on February 26, 1996, now abandoned, which is a Continuation of Application Serial No. 08/433,784, filed on May 3, 1995, now abandoned, which is a Division of Application Serial No. 08/370,051, filed on January 9, 1995, now Patent No. 5,525,695, which is a Division of Application Serial No. 08/044,426, filed on April 7, 1993, now Patent No. 5,380,810, which is a Division of Application Serial No. 07/776,130, filed October 15, 1991, now Patent No. 5,272,236.--

On page 36 replace the paragraph starting on line 17 with the following paragraph:

--The ethylene (4) and the hydrogen (5) are combined into one stream (15) before being introduced into the diluent mixture (3). Typically, the diluent mixture comprises a mixture of C_8-C_{10} saturated hydrocarbons (1), (e.g., Isopar® E, made by Exxon) and the comonomer(s) (2). For examples 1-4, the comonomer is 1-octene. The reactor feed mixture (6) is continuously injected into the reactor (9). The metal complex (7) and the cocatalyst (8) (the cocatalyst is tris(pentafluorophenyl)borane for Examples 1-4 herein which forms the ionic catalyst insitu) are combined into a single stream and also continuously injected into the reactor. Sufficient residence time is allowed for the metal complex and cocatalyst to react to the desired extent for use in the polymerization reactions, at least about 10 seconds. For the polymerization reactors of Examples 1-4, the reactor pressure is held constant at about 490 psig. Ethylene content of the reactor, after reaching steady state, is maintained below about 8 percent.--